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4 Effects of red blood cell aggregation on
5 microparticle wall adhesion in circular
6 microchannels

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20 **ABSTRACT**

21 The wall adhesion of 1 μm microparticles in human blood was studied in circular microchannels.
22 The level of particle wall adhesion was measured for varying levels of shear rate and varying degrees of
23 red blood cell aggregation, which was modulated by the addition of macromolecule dextran 500. The blood
24 preparations were injected into PDMS microfluidic devices that were modified to have circular channels,
25 better matching the geometry of physiological microcirculation compared to square channels or Couette
26 flow systems. The circular walls of the microchannels were embedded with biotinylated phospholipids to
27 which marginating microspheres coated with streptavidin bound. The particle wall adhesion was evaluated
28 by counting the particles that adhered to the channel's wall after flushing the channel. Blood preparations
29 of five dextran concentrations (including baseline case of 0%) were tested for four flow velocities, to
30 quantify the effects of aggregation for varying shear rate. It was found that the level of particle wall adhesion
31 was positively correlated with the level of RBC aggregation, particularly at low shear rates, when
32 aggregation was enhanced. The particle adhesion was especially enhanced at aggregation levels in the range
33 of physiological aggregation levels of whole blood, suggesting that RBC aggregation plays an important
34 role in the dynamics of platelets and leukocytes *in vivo*.

36 **1 INTRODUCTION**

37 Margination, the radial migration of particles in a channel flow towards the channel walls, which could
38 result in the attachment of the particles to the wall, is an important feature of the microcirculation. The
39 margination of platelets and leucocytes towards the vessel endothelium, and by extension their adhesion, is
40 essential to their functions in wound healing, maintaining homeostasis, and the body's immune response to
41 inflammation and infection [1]. Margination and wall adhesion are also important to drug delivery, since
42 drug-carrying particles must come into close proximity with the vessel walls in order to be absorbed by the
43 tissue. An advanced understanding of the mechanisms involved in particle margination and adhesion *in*

44 *in vivo* could lead to improved drug design for targeted delivery [2]. Margination also has important
45 applications *in vitro*; some lab-on-a-chip devices, for example, use the phenomenon to separate cells such
46 as different blood components, or healthy cells from diseased ones [3,4].

47 Particle margination could be assessed by reporting the distribution of the particles across the channel
48 radius, i.e. the local particle concentration [ref]. Usually, in blood the concentration is measured close the
49 wall as the core of the vessel is occupied by RBCs. Such measurements require the use of fluorescent
50 confocal microscopy. An alternative is to measure the particles that have attached to the wall, which is
51 correlated to the particle margination[ref].

52 Margination is a complicated physical phenomenon influenced by the size, shape, density and stiffness
53 of the marginating particles, as well as by the fluid shear rate, vessel geometry, and the concentration and
54 aggregation tendency of the surrounding red blood cells [1]. While leukocytes, platelets and nanoparticles
55 have all been shown to marginate in blood flow, their marginating behaviours are not affected equally by
56 the blood flow variables. Margination is the result of a balance of forces acting on the particles - namely
57 gravity, buoyancy, fluid drag, van der Waals and Brownian forces - causing their net lateral movement
58 away from fluid streamlines [1]. As particle size increases, this force balance changes, with gravity and
59 fluid drag becoming increasingly important, whereas for very small particles (<500 nm) Brownian motion
60 and colloidal forces dominate. Charoenphol *et al.* found that for spheres 0.5 to 10 μm in diameter,
61 margination increased with increasing particle size [5]. In general, non-spherical particles have a higher
62 tendency to marginate than spherical ones [1].

63 Nobis *et al.* found that leukocyte margination was negatively correlated with shear rate [6]. Conversely,
64 Tilles and Eckstein, and Aarts *et al.* found that the margination of smaller platelets or beads in RBC
65 suspensions flowing in glass capillaries increased with shear rate [7,8]. Yeh. and Eckstein , on the other
66 hand, found that in high hematocrit suspensions (H=40%), the margination of platelet-sized spheres was
67 maximum at some optimal shear rate, suggesting that the shear-marginating relationship is more complex
68 [9].

69 From early experiments of blood in glass capillaries, Vejlens was the first to correlate the margination
70 of leukocytes with RBC aggregation [10]. While it has been found that RBC aggregation is not necessary
71 for WBC margination to occur [11,12], from their 2D numerical simulation of Fedosov showed that it does
72 strengthen it [11]. Likewise, Pearson and Lipowsky found RBC aggregation to be positively correlated
73 with leukocyte margination in venules in rat mesentery [13]. They found this effect was most prominent at
74 higher hematocrits and shear rates, and attributed it to tighter RBC packing when aggregated (i.e. a less
75 dispersed RBC core) which inhibited the white blood cells from lifting off away from the wall. This finding
76 may explain a mechanism of the body's immune response: inflammatory conditions *in vivo* have been found
77 to promote abnormal hyper RBC aggregation – this correlation suggests that this may be in order to force
78 more leukocytes toward the endothelium where they are needed to respond to the inflammation.

79 The effect of RBC aggregation on platelet margination is less conclusive. Woldhuis *et al.* found that by
80 increasing RBC aggregation in rabbits (by addition of dextran 500), platelets became more centrally
81 distributed in arterioles; i.e., opposite to the findings for leukocytes, platelet margination was negatively
82 correlated with RBC aggregation [14]. They found no correlation, however, in venules. Guilbert *et al.* ,
83 however, conversely found that in Couette flow, 2 μm spheres (comparable in size to platelets) adhered
84 more to the Couette wall with increasing RBC aggregation [15]. This result was consistent for three
85 hematocrits (20%, 40%, 60%), and two shear rates tested (2 s^{-1} and 10 s^{-1}). These contrasting results raise
86 questions about the effects of other factors including the shape and flexibility of platelets compared to
87 sphere surrogates, the endothelial receptors and strength of bond, and the effects of the channel geometry
88 and associated shear profiles. It is necessary to investigate these variables independently in order to
89 delineate their effects.

90 Jain and Munn showed that channel size indeed affects the marginating behaviour of WBCs, with
91 margination decreasing with increasing channel width in rectangular channels [16] (this is consistent with
92 findings of Goldsmith and Spain in glass capillaries [17]), and increasing at sudden expansions. Yang *et*
93 *al.* reported the effect of channel cross-sectional geometry on leukocyte margination and found that

94 leukocyte trajectories were drastically influenced by the channel cross-section when flowing in bifurcating
95 microchannels with either rectangular or rounded cross-sections [18]. In the rectangular channels, the
96 WBCs margined preferentially towards the corners, which effected their distribution between the
97 bifurcating branches. This finding emphasized the importance of modelling anatomically accurate channel
98 geometries when modeling microcirculatory flows.

99 These effects of varying geometry on the margination of different particle sizes are coupled with the
100 differences in shear rate profiles associated with the geometry, which as discussed above, have a strong
101 influence on particle margination. For example, leukocytes have been found to marginate more in post-
102 capillary venules than in arterioles, whereas platelets were found to marginate more in arterioles [2]. This
103 may be a consequence of the sensitivity of the different particle characteristics (size, shape and flexibility)
104 to the different shear rates and geometries present in arterioles vs. venules. RBC aggregation is another
105 coupled variable, as it increases at low shear rates and is inhibited at shear rates greater than $100\text{-}120\text{ s}^{-1}$
106 [19].

107 In summary, with many variables at play, the detailed mechanisms of micro-particle margination remain
108 unclear. No study has been done to our knowledge investigating the effects of RBC aggregation on platelet-
109 sized particles in circular microchannels. Assuming wall adhesion being proportional to the margination,
110 the objectives of this research are to quantify the effects of RBC aggregation on micro-particle wall
111 adhesion ($1\mu\text{m}$ spheres) under physiological arteriole flow conditions within round microchannels, under
112 varying physiological levels of shear rate. methods

113 *1.1 Channel fabrication*

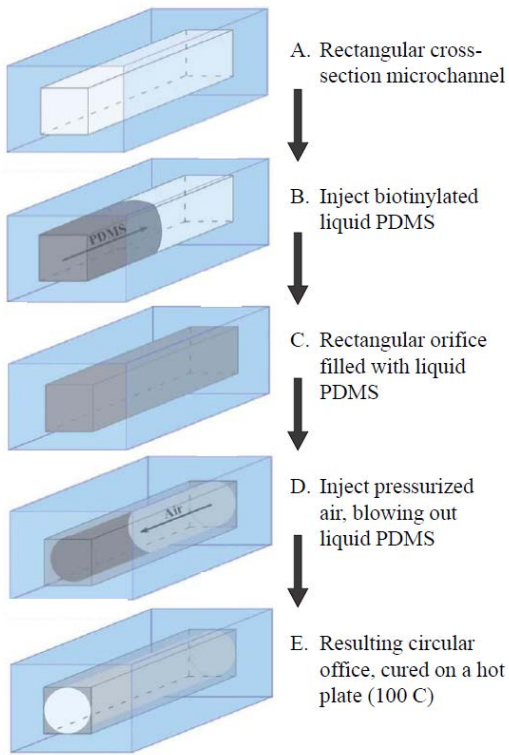
114 Circular microchannels were fabricated in PDMS. Using a method introduced by Yang *et al.* [18], this
115 was done by first fabricating channels having approximately square cross-sections, which were used as
116 scaffolds filled in a second step to have circular cross-sections (Figure 1). The liquid PDMS used in the
117 second step was mixed with biotinylated phospholipids, embedding the channel walls with functionalized

118 biotin groups to which the marginating microspheres, coated in streptavidin, would strongly bind. The
119 square scaffold channels were fabricated using a standard procedure, outlined briefly in the following. The
120 resulting channel geometries on the master mold had dimensions 1.00 cm long, 106 μm in height and 116
121 μm in width.

122 PDMS pre-polymer and a curing agent were mixed together at a ratio of 10:1. The mixture was
123 degassed (72 kPa for one hour) and poured onto the channel master and baked on a hot plate (30 min at
124 135°C). Once removed from the mold, the PDMS was cut into individual chips and holes were punched
125 through at the inlets and outlets. The cast PDMS sections were then bonded to another flat piece of PDMS
126 using an Oxygen Plasma etcher (PE-50: Plasma Etch Inc., Carson City, USA) to enclose the channels.

127 The square PDMS microchannels were then filled with biotinylated liquid PDMS to create rounded
128 channels. One milliliter of liquid PDMS was combined with 7.5 μL of a 5 mg/mL phospholipid–chloroform
129 solution. The biotinylated liquid PDMS was injected into the square channels with a syringe. A stream of
130 compressed air (5 psi/cm) was injected through the microchannels, while curing on a hot plate at 100°C for
131 20 minutes, forcing the liquid PDMS out and leaving a circular channel. In order to fully cure the deposited
132 PDMS coating, the channel was baked for an additional 20 minutes at 100°C with no compressed airflow.

133 The channel diameters were measured by cutting off the end portion of each channel, and imaging
134 its cross section under the microscope. The average diameter D was taken as the average of two orthogonal
135 measurements, D_1 and D_2 . Over 50% of the channels that were made using this procedure had near-circular
136 cross-sections (Figure 2 (b)), as judged by the ratios of D_1/D_2 . This result was considered satisfactory, given
137 that individual channels were examined prior to being used for the experiments to ensure that they were
138 circular. The average channel diameter was $85 \pm 7\mu\text{m}$.



139

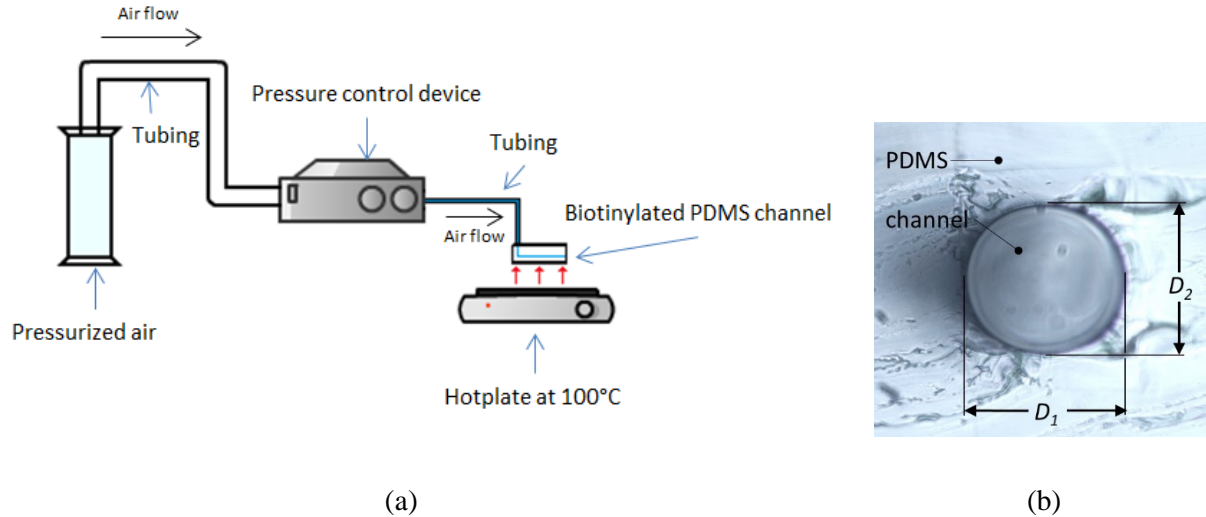
140 Figure 1. Steps in creating a round channel in PDMS. Modified from Yang *et al.* [18].

141 *1.2 Measurement of particle adhesion*

142 Human blood was collected from volunteers by Gamma Dynacare laboratories (Ethics reference
 143 number: H11-13-06). A standard procedure for blood separation was used: the blood samples were
 144 centrifuged at 3000 rpm for 10 minutes, the plasma and the buffy coat were extracted and discarded, and
 145 phosphate buffered saline (PBS) was added to the remaining red blood cells to wash them. This was
 146 repeated twice more. The cleaned RBCs were suspended in a solution of PBS with 27% v/v of Optiprep™
 147 Density Gradient Medium (MFCD00867965: Sigma-Aldrich, St. Louis, USA) to achieve hematocrits of
 148 10%. The Optiprep™ was added to increase the density of the suspending medium to minimize
 149 sedimentation during the experiment. Five different solutions were prepared from each suspension mixture,
 150 having 0%, 0.5%, 1.0%, 1.5% and 2.0% w/v concentrations of dextran 500 (AAJ63702-22: VWR
 151 International, Radnor, USA).

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155

156 Figure 2. (a) Diagram of air pressure set-up used to create circular channels: Pressurized air first leaves its storage and flows into
157 the pressure control device, which ejects air at a controlled pressure of 5psi per cm of channel length. The controlled air flows into
158 the channel while it is heated at 100°C and pushes the injected liquid biotinylated PDMS out to make a circular channel. (b) Cross-
159 section of a typical round microchannel, imaged under a microscope. Characteristic diameter D was taken as the average of the two
160 orthogonal diameter measurements, D_1 and D_2 .

161 Fluorescent particles, 1 μm average diameter, coated with streptavidin (Excitation: 480nm, Emission:
162 520nm, CP01F-12884: Bangs Laboratories, Fishers, USA) were added to the blood suspensions at a
163 concentration of 27 μL of particle solution per mL of sample fluid. The blood preparations were sonicated
164 for three minutes (ultrasonic bath RK-08848-10: Cole-Parmer, Montreal, Canada) to break up any clumps
165 of particles, to ensure that the particles would be dispersed homogeneously throughout the solution. These
166 particles were chosen for their comparable size to platelets.

167 RBC aggregation levels were measured for each suspension of varying dextran concentration under
168 static conditions using an aggregometer (RheoScan-AnD 300 System: RheoMeditech Inc., Seoul, Korea).
169 Because the aggregometer uses light intensity passing through the sample to measure the aggregation level,
170 the hematocrit of the samples must be near physiological levels to obtain an accurate reading: for samples

171 having too low hematocrit, too much light would pass through the sample, resulting in overexposure and
172 inaccurate readings. For this reason, we used suspensions of 45% hematocrit to establish the relationship
173 between dextran concentration and aggregation, instead of the 10% hematocrit used in the flow experiment.
174 We also note that false positive measurements were obtained for samples of 0% dextran, as the
175 measurement mechanism requires some level of aggregation to operate; however, unlike the aggregating
176 samples, for which the measured light intensity passing through the sample increased in time as the RBCs
177 aggregated, the measured light intensity for the 0% samples continually decreased. For this reason, the
178 aggregation indices of the 0% dextran samples were set to zero.

179 A syringe pump (Nexus 3000: Chemyx Inc., Stafford, USA) controlled the flow rate of the blood
180 samples through the microchannels. After the blood preparation was flowed through and the channel was
181 cleaned with PBS, the channel was examined under an LED fluorescent microscope (Axio Lab.A1: Carl
182 Zeiss AG, Oberkochen, Germany) to image the channel and count the fluorescent particles that remained
183 adhered to the walls. Particles were imaged under a 10x magnification lens using a florescent filter
184 (excitation band pass 450-490 nm, emission low pass 515 nm).

185 The observations were made 0.5 mm from the inlet to avoid any effects due to the specificity of the
186 flow at the entrance. Two images were taken at the same location in each channel, using two different focal
187 points within the channel to ensure that all adhered particles were represented and in focus between the two
188 images (Figure 3 (a) and (b)). The two images were overlaid to produce a combined image (Figure 3(c)).
189 This was then converted to an 8-bit black and white image, sharpened, and converted into a binary image
190 using a threshold that was manually set so that only the particles were visible. Finally, the black and white
191 values were inverted (Figure 3 (d)). A particle counting algorithm in ImageJ was used to extract the size
192 and number of the bright spots in the image. Several sets of images were counted manually to verify the
193 accuracy of the ImageJ particle counting macro, and in all cases, the results differed by less than 10%, and
194 the result from ImageJ was used.

195 The experiment was performed for four different target mean flow velocities: $v = 0, 1.0, 2.0, 3.0,$
 196 and 6.0 mm/s. The flow rates used to program the syringe pump were calculated for each channel to achieve
 197 the desired mean velocity as $Q = \pi v D^2 / 4$, where D is the measured diameter of the channel in use.

198 Each blood sample was flowed through a channel for one minute at the flow rate calculated for that
 199 channel to achieve the desired velocity. All combinations of flow velocity and dextran concentration were
 200 each repeated five to eight times. Each test was performed in a new, clean channel that was fabricated no
 201 more than 48 hours beforehand.

202 As measures of particle margination, we examined the absolute particle counts for each condition,
 203 normalized by the averaged counts obtained from the baseline 0% dextran samples. We additionally defined
 204 a non-dimensional adhesion coefficient C_a , normalized by the particle flux through the channel as:

205 $C_a = \frac{c_w}{J_p}$, where c_w is rate of particle capture at the wall per unit surface area in particles/(s.m²), $J_p =$

206 $\frac{\phi Q}{\vartheta_p \pi R^2}$ is the flux of particles through the capillary cross section, also in particles/(s.m²), ϕ is the volume

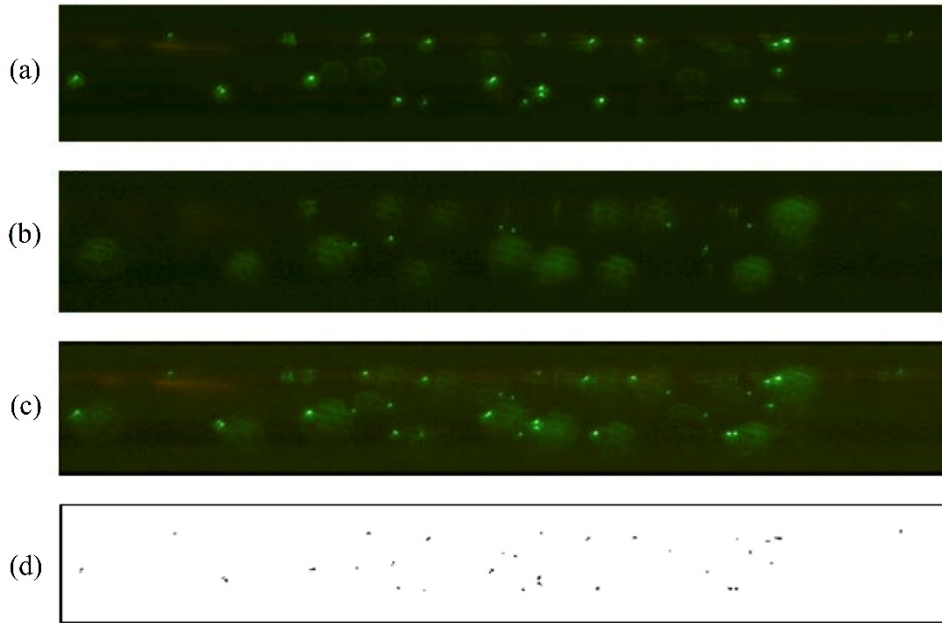
207 fraction of particles, Q the flow rate, ϑ_p the volume of a single particle, and R the capillary radius. Assuming

208 a steady condition, C_a was estimated after flowing the solution during $T=1$ min as:

209 $C_a = \frac{\int_0^T c_w dt}{\int_0^T J_p dt}$, where $\int_0^T c_w dt$ is the total count of particles per unit of surface at $t=T$ and $\int_0^T J_p dt$ is the total

210 count of particles that cross the capillary section during $t=T$. For each trial, a shear rate metric γ (s⁻¹) was

211 calculated from the channel diameter D and average flow velocity v as $\gamma = 4v/D$.



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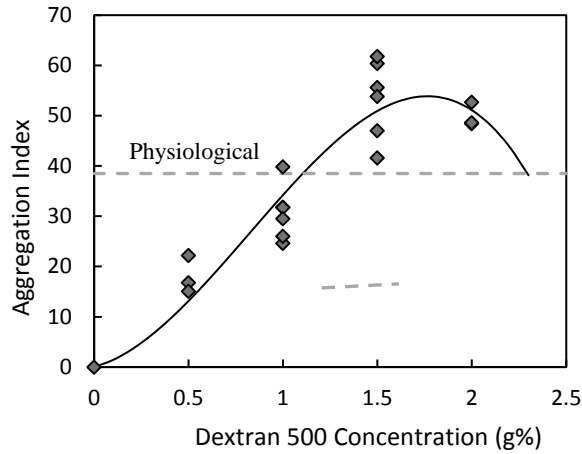
213 Figure 3. Image processing method used to count particle adhering to channel walls: (a) and (b) original two images taken at
214 different focal distances within the channel; (c) the combined image; (d) the post-processed image used for particle counting.

215 **2 RESULTS AND DISCUSSION**

216 *2.1 Effect of dextran on RBC Aggregation*

217 The effect of dextran 500 on the RBC aggregation levels was found to be similar to that previously
218 reported [19]: aggregation was found to increase with increasing dextran concentration up to the 1.5%
219 samples, beyond which it decreased. Fitting a third order polynomial to the measurements (Figure 4), the
220 peak aggregation was more precisely estimated to correspond with concentrations of 1.76% dextran, which
221 is within the range of values previously reported [13,19,20]. The averaged aggregation indices of the
222 different dextran concentrations are reported in Table 1, with the physiological value reported by Baskurt
223 *et al.* listed for reference [19].

224



225

226 Figure 4. Aggregation index vs. concentration of dextran 500. A third order polynomial is fitted to the data (continue line).

227 Table 1. Average aggregation indices for increasing dextran concentration. *Physiological value from [19] for the same type of
 228 aggregometer..

Dextran Concentrations	Aggregation Index
0.0%	0*
0.5%	18.0 ± 3.7
1.0%	30.6 ± 5.4
1.5%	53.4 ± 7.8
2.0%	49.9 ± 2.4
Physiological*	38.5 ± 2.2

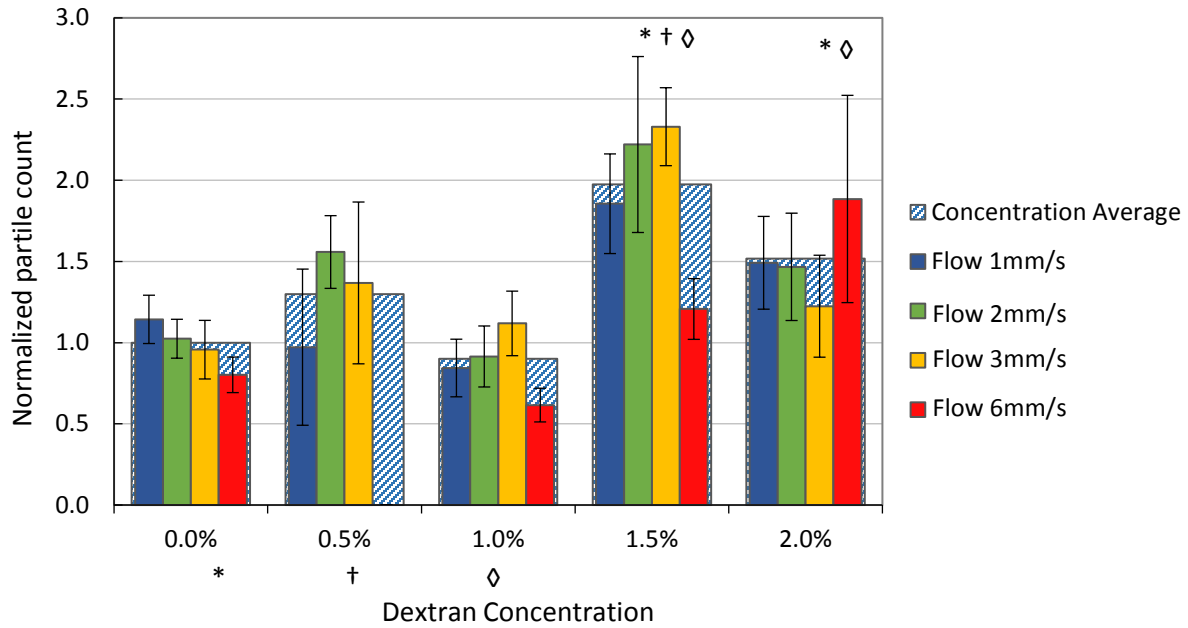
229 **2.2 Particle Adherence**

230 The average particle counts, normalized by the averaged results for the 0% dextran concentrations, are
 231 presented in Figure 5 for all dextran concentrations and flow velocities tested. The results averaged across
 232 the different flow velocities for each dextran concentration are also shown here as hatched bars. Following
 233 the same trend of aggregation index vs. dextran concentration (Figure 4), with the exception of the 1%

234 dextran concentration, average particle adherence increases up to 1.5% dextran, and decreases for the 2%
235 dextran samples. Comparing these averaged results using two-tailed t-tests, particles in the preparations
236 that had levels of aggregation below physiological levels (0%, 0.5% and 1.0% dextran) were on average
237 significantly less likely to marginate compared to those in the samples having aggregation levels higher
238 than physiological (1.5% and 2.0% dextran).

239 This relation between aggregation and particle adherence is further illustrated by Figure 6, in which the
240 normalized adhesion coefficients C_a are plotted against the aggregation indices for the corresponding
241 samples. These results are presented for the lowest flow velocity $v=1.0$ mm/s, as well as the averaged C_a
242 values for velocities 1, 2, and 3 mm/s. The adhesion coefficient is positively correlated with aggregation
243 index, illustrated by lines of best fit. The slope of the fitted line is higher for the results of the lowest velocity
244 than for those of the averaged velocities, indicating that margination is more sensitive to the aggregation
245 level at lower velocities, and the corresponding lower levels of shear. This result is not surprising, given
246 that RBC aggregation decreases and is eventually inhibited as shear rate increases, so its influence on
247 margination would also be expected to dissipate with increasing velocities and shear.

248



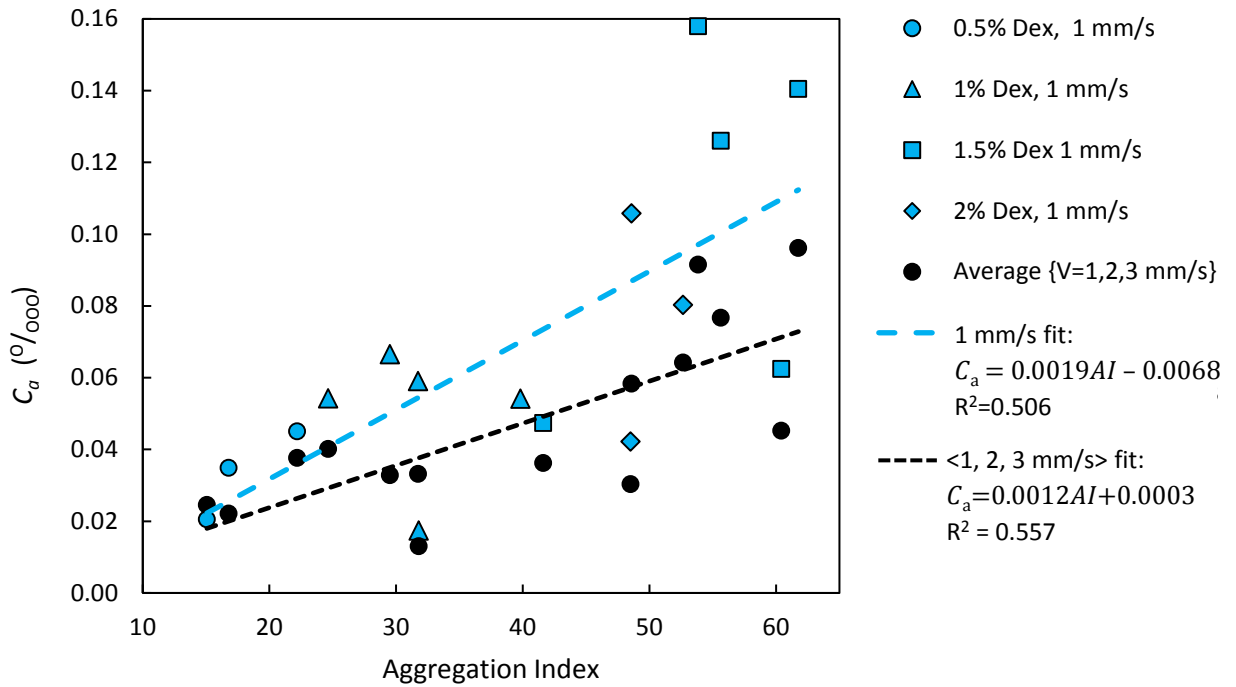
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250 Figure 5. Averaged normalized counts of binding microparticles for each concentration of dextran 500 and each flow velocity.

251 Particle counts were normalized by the averaged result for the 0% dextran solution (all velocities). Hatched bars present particle

252 counts averaged across all velocities for each dextran concentration. *†◇ above a bar signifies statistically significant difference

253 with the averaged result for the respective dextran concentration ($p < 0.05$).



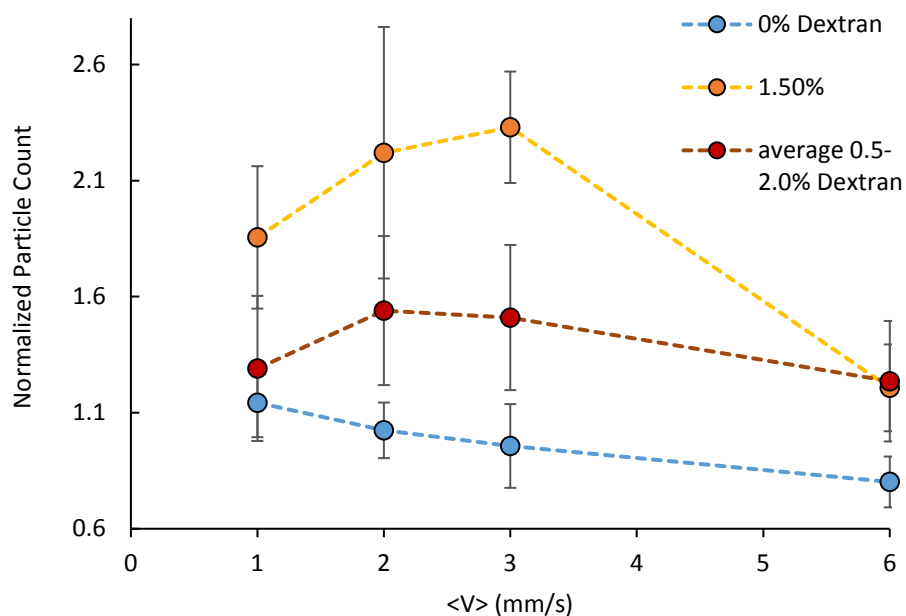
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256 Figure 6. Adhesion coefficient C_a vs. corresponding aggregation index for lowest flow $v=1$ mm/s along with averaged results for
 257 $v=1, 2,$ and 3 mm/s. Lines of best fit are presented by dashed lines. ‰ signifies “per ten thousand”, i.e. reflects the number of
 258 particles attached per 10,000 particles injected.

259

260 From the results of all particle counts shown in Figure 5, we see that the effects of flow velocity on
 261 particle adherence vary depending on the dextran concentration. Figure 7 compares the effect of flow
 262 velocity on particle adherence in blood samples with no aggregation (0% dextran), maximum aggregation
 263 (1.5% dextran) along with the average for all of the aggregating samples (0.5-2.0% dextran). For the non-
 264 aggregating samples, there is a moderate negative trend, with particle adherence decreasing monotonically
 265 by 30% from velocities 1 mm/s to 6 mm/s. This trend corresponds with other findings that show a negative
 266 correlation between shear rate and margination [15] and may be explained by higher by shear forces at the
 267 wall that “wash away” some particles and the increase of shear-induced diffusion, which displaces the
 268 particles toward the center. According to Taisuke Ota, a single biotin molecule (ligand) forms a bond with

269 a streptavidin molecule (receptor) with the rupture force between 3.6 and 5.4 pN [REF]. For the presented
 270 experiments, the drag force applied by the flow on the spherical particles touching the wall was estimated
 271 to fall between 0.7 and 4.4 pN (Stokes flow, viscosity 3.5mPa.s). According to this analysis, the shear is
 272 likely responsible for a significant amount of particle detachment.



273
 274 Figure 7. Particle Margination vs. flow velocity. Normalized averaged particle counts vs. average flow velocity for: zero
 275 aggregation (0% dextran), maximum aggregation (1.5% dextran) and average for all aggregating samples (0.5-2% dextran).

276 With the presence of RBC aggregation, the effect of flow velocity on the number of captured particles
 277 was significantly altered: in addition to having higher levels of particle adherence overall, unlike for the
 278 non-aggregating samples, the relationship for the aggregating samples (1.5% and average concentration) is
 279 non-monotonic. Particle adherence increases up to some optimal velocity, beyond which it decreases. For
 280 the maximum aggregation level (1.5% dextran), margination was greatest at $v=3$ mm/s. For the averaged
 281 dextran concentrations it was greatest at $v=2$ mm/s.

282 When plotting the adhesion coefficient that has been normalized by the particle flux, however (Figure
 283 8), we see that this indicator of margination decreases monotonically with increasing shear rate. This reveals
 284 that the maxima observed for aggregating samples in Figure 7 was indeed, consequence of the increased

285 particle flux associated with the increased flow rates. For aggregating samples, the effects of aggregation,
286 coupled with the increased particle flux, resulted in a net increase in captured particles up to some critical
287 velocity (Figure 7). Above this velocity, the elevated shear forces that inhibit margination also broke up
288 aggregates, eliminating their pro-margination influence, and the number of captured particles decreased. It
289 is reasonable that the critical velocity for maximum particle count was highest for the highest aggregation
290 level, because for these samples, aggregates would have been larger, on average, and more resistant against
291 shear to break apart, thus prolonging the aggregates influence on margination up to higher flow velocities.

292 The averaged values of C_a plotted in Figure 8 (c) further show that at low shear rates ($<150 \text{ s}^{-1}$) higher
293 levels of aggregation are associated with significant increases in margination. This effect diminishes as the
294 shear rate increases. Again, this result was expected, as at shear rates above $100\text{-}120 \text{ s}^{-1}$, RBC aggregation
295 is inhibited and disaggregation occurs [19]. For each concentration of dextran, the dimensionless adhesion
296 coefficients were plotted against the inverse shear rate and fitted with linear regression as $C_a = \alpha/\gamma$, where α
297 is the experimental fit coefficient (Graphs not shown here). The fit coefficients and R^2 values for the five
298 different aggregation levels are listed in Table 2, and the fitted trends for the 0% and 1.5% dextran
299 concentrations are plotted as dashed lines, along with the averaged results in Figure 8 (c). The fit coefficient
300 α represents the sensitivity of the marginating behaviour to the aggregation level. It is relatively constant
301 for the lower aggregation levels (0-1% dextran) but increases significantly in the higher dextran
302 concentrations ($>1\%$) as the mean aggregation index increases (Figure 9). In other words, as aggregation
303 levels increase to near the range of physiological levels, its influence on margination is heightened,
304 particularly at low levels of shear rate. This is presumably due to the larger aggregate sizes associated with
305 the higher aggregation indices and enabled by the lower levels of shear.

306 For both the red blood cells and particles, the Péclet numbers are high (~ 1000), and the particle
307 Reynolds numbers are low (~ 0.0001). This suggests that shear-induced migration dominates Brownian
308 diffusion and inertial lift for these conditions [21]. For monodisperse particles, the shear-induced diffusion
309 is proportional to the product γD_p^2 , where D_p is the particle diameter [22]. As the RBCs and RBC aggregates

310 have effective diameters considerably larger than the $1\mu\text{m}$ particles, their migration toward the center is
311 greater. Therefore, with the core of the vessel predominantly occupied by the RBCs, the particles are left
312 close to the wall. The net effect of shear can be interpreted as a combination of the increase of shear force
313 at the wall that “washes away” some particles and the increase of shear-induced diffusion, which displaces
314 the particles toward the center.

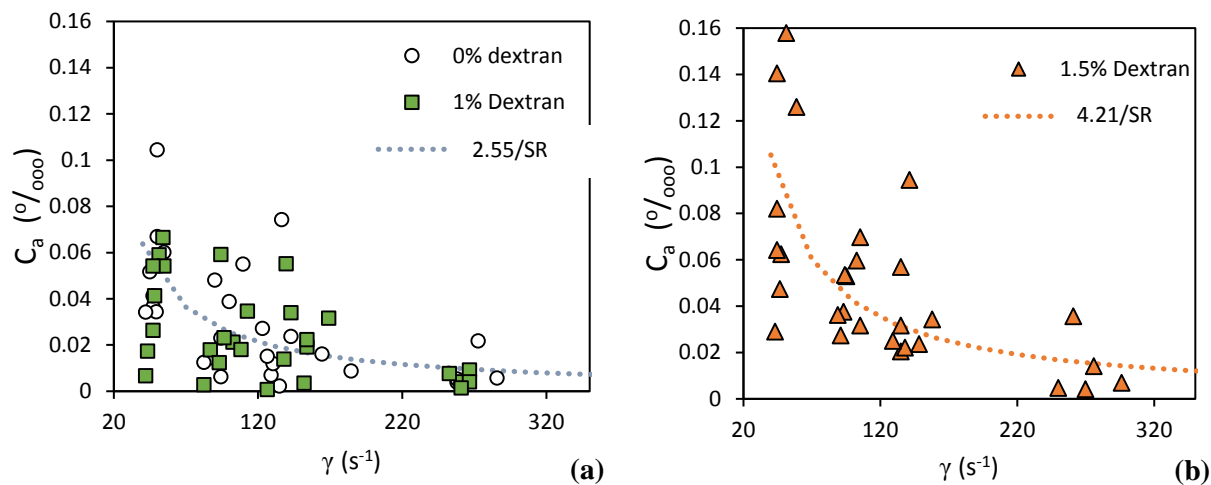
315 While the behaviour of polydisperse solutions is not yet fully understood, it has been shown that shear-
316 induced migration enables separation of the feed flow [23]. This suggests that RBC aggregation - which
317 increases the effective size of the “blood particles”- enhances segregation of the micro-particles, promoting
318 their attachment to the wall.

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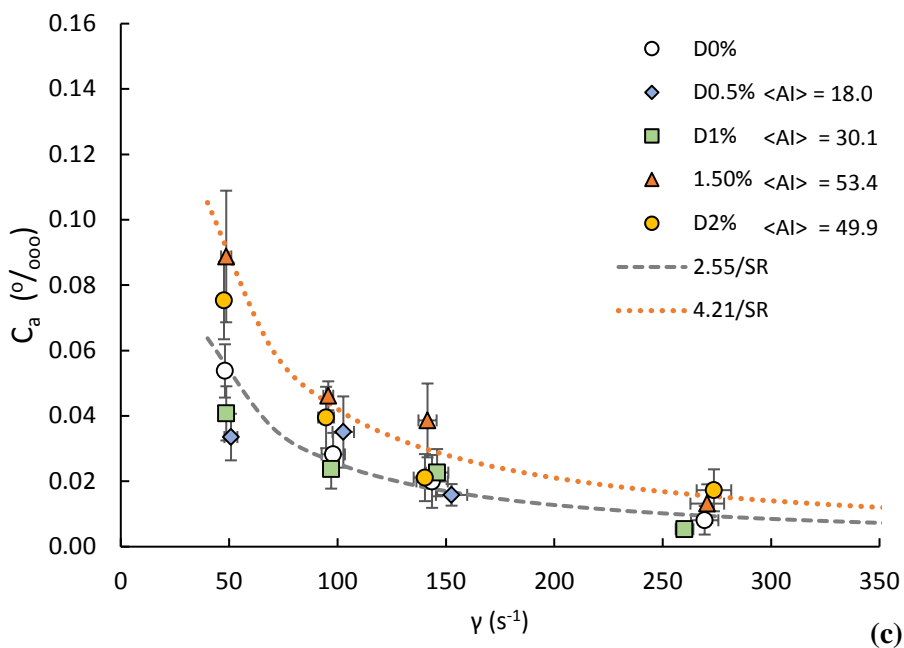
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325 Figure 8. Normalized adhesion coefficient C_a vs. shear rate: (a) for 0% and 1% dextran concentrations; (b) for 1.5% dextran
326 concentration; (c) averaged results for all dextran concentrations. ‰ signifies “per ten thousand”, i.e. reflects the number of
327 particles attached per 10,000 particles injected.

328

329

Table 2: adhesion fit coefficient (α) versus *mean* aggregation indices. * Aggregation index of the 0% dextran samples were set to zero

dextran (w/v)	Mean Aggregation Index	α	R ²	Two-tailed Probability
0%	0*	2.55	0.43	p=0.00004 (N=32)
0.5%	18.0	2.07	0.69	(N=9)
1%	30.6	2.03	0.33	p=0.00125 (N=29)
1.5%	53.4	4.21	0.50	p=0.00002 (N=29)
2%	49.9	3.47	0.71	p=0.000003 (N=20)

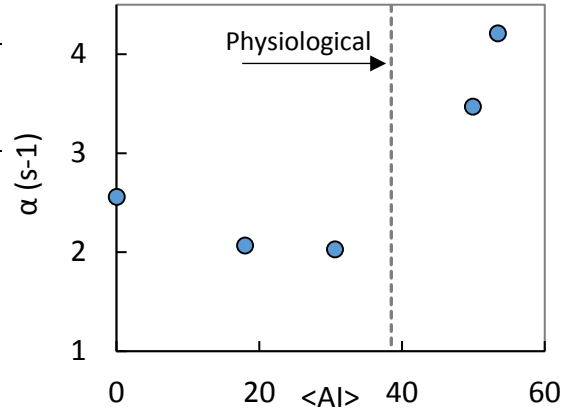


Figure 9. Alpha factor vs. mean aggregation index corresponding to Dextran concentration 0 to 2%.

In this study, we have used particle adhesion as an indicator of particle margination. We note that while closely related to margination, particle adhesion is an imperfect measure of it, as it does not account for particles that may become detached from the wall due to increasing fluid drag or collisions with RBC aggregates [24], or the characteristics of the molecular bonds with receptors in the endothelium [1]. In future studies, investigators may measure the particle distribution in the tube as a more direct measure of margination. We also note that this study of rigid spheres does not account for cell flexibility or the shape of irregular particles such as platelets, and that these variables could account for the contradicting results regarding margination of platelets and similar sized spheres reported in literature. Here, we established the effect of RBC aggregation on the margination of 1 μm rigid spheres within round channels under varying shear rate in the range of physiological conditions. These results may help to delineate the effects of specific platelet characteristics, which may be investigated in future studies. In addition, according to Muller et al. [Muller] particle margination strongly depends on how well particles fit within a cell free layer. Considering

this and that RBC aggregation is known to increase the cell free layer thickness [5], further optimization of particle size should take into account the aggregability of the blood.

3 CONCLUSIONS

The effects of RBC aggregation level on the margination of 1 μm spheres has been quantified within round microchannels (85 μm) under varying physiological levels of shear rate. For the non-aggregating samples (0% dextran) the absolute numbers of captured particles decreased with increasing flow velocity, but for the aggregating samples, particle capture was significantly higher and exhibited a local maximum for a critical velocity. A non-dimensional adhesion coefficient was defined to account for the increased particle flux associated with higher flow rates, and exhibited a monotonic decrease with shear rate for all aggregation levels. Increase in aggregation level resulted in a significant increase in margination for both absolute and dimensionless indicators, particularly at low levels of shear rate ($<150 \text{ s}^{-1}$) under which aggregation was strongest. This finding agrees with those of other studies that examined the effect of aggregation on margination within different channel geometries (e.g. a Couette cylinder [25] or parallel plate flow chamber [26]). Margination was found to be especially sensitive to aggregation level in the range of physiological aggregation levels of whole blood (most notably for the 1.5% dextran concentration). This indicates that aggregation plays an important role in physiological margination. It has already been shown that aggregation plays an important role in the human body's immune system [27], and the presented results indicate that one mechanism by which it does this is by increasing margination, which can help platelets and immune cells travel to the site of inflammation to support the healing and immune defense process. This potentially explains why an increase in aggregation is so often observed in different pathological conditions. These findings could be used better understand the roles of aggregation and margination in the body and their importance toward inflammation and immune response.

Conflict of interest

The authors have no conflicts of interest.

Ethical approval

The study was conducted with the with the approval of the University of Ottawa ethics committee (H11-13-06)

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